Foam Filtration Reflection Report 1

Foam Filtration Reflection Report Primary Authors: Leila Zheng Melissa Shinbein Kevin Wong Catherine Hanna

> Primary Editor: Sarah Stodter

AguaClara Reflection Report Cornell University School of Civil & Environmental Engineering Ithaca, NY 14853-3501

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Abstract

Current ly, after underg oing filtratio n and sedime ntation, an AguaCl ara plant can produce effluent water with a turbidit y of approxi mately five NTU (Nephel ometric Turbidi ty Units). By adding foam filtratio n to the plants, the group hopes to reduce this effluent turbidit y to below one NTU.

Last semester, the foam filtration team tested the filtering capacity of foam using a shallow filter (3 inch depth) and flow rates comparable to a rapid sand filter (1-3mm/s). While acceptable performance could be achieved under the right conditions (alum dose, low flow rate), it was found the filter could not be run with a horizontal flow direction. This inability to manipulate the geometry of the filter resulted in a large required plan area, and it became necessary to test for different filtering conditions.

This semester, it was decided to manipulate the geometry of the foam filter by increasing both the down flow velocity and filter depth. Research over the last two weeks has proven this to be an effective method, and a performance study will be conducted throughout the summer to determine the parameters under which effective performance can be achieved.

Introduction

The filtration team's objective is to design a filtration unit that can reliably treat the current effluent water with a turbidity of about 5 NTU to a turbidity of less than 1 NTU. Most of the current filtration systems use sand as the porous media, and very little information is present regarding foam filtration. Rather than using the traditional method of sand filtration, our research will focus on the filtering capacity of polyurethane foam material.

Members of a previous foam filtration team have tested the filtering capacity of foam under worst-case scenarios, which involved filtering water with un-flocculated clay particles. To simulate conditions that more resemble those of an AguaClara plant, an alum dosing system and rapid mix tube were added to the experimental apparatus. The first experiment, which used an alum dose of 25 mg/L (a very high and unrealistic alum dose), resulted in effluent turbidities of less than 1 and pC* of .9 when flow rates of 2 mm/s or less were used. This demonstrated that filter performance declined with increased flow rates. This was explained by the idea that at lower flow rates, the foam was able to capture even the smallest particles that would have been made sticky by alum, but as flow rates increased, it became increasingly difficult for the foam to capture smaller particles. The next experiment used an alum dose of 1.5 mg/L, a value chosen based on the assumption that 5% of the particles remained when originally exposed to a 30 mg/L alum dose. The minimum turbidities achieved were not as low as that achieved with a higher alum dose. This can be attributed to the fact that with lower alum dose, not as many of the smaller particles are made larger from contact with alum. Subsequent experiments compared performance from 3-in. to 1-in. foam depth, and demonstrated that foam filtration acted as a function of depth, rather than surface area.

The feasibility of horizontal filtration, in which raw water would flow horizontally through a vertically placed filter, was tested. It was shown that horizontal filtration could not provide the standards of achieving a .9 pC^* within a reasonable timeframe (pC^* of .7 after 20 hrs). Rotation of the column in a subsequent experiment showed that a turbidity gradient had developed over the depth of the filter, with very turbid water going through the bottom and less turbid water going through the top. This turbidity gradient is likely to contribute to the observed decrease in performance when compared to vertical filtration.

A number of experiments utilizing foam with different pore sizes and flow rates were conducted. The first experimental set-up utilized 60-ppi foam, while the second used 90-ppi foam. With 60-ppi foam, a significant level of colloid removal was achieved with a pC* of .6 at 1.15 mm/s and pC* of .4 at 2.31 mm/s. It would be optimal to achieve a pC* of .9, so consequently, foam with a higher ppi was investigated. Using flow rates varying from .57 to 2.89 mm/s, an effluent turbidity of 1.5 NTU and pC* of .55 were found, which is similar to that of the 60-ppi foam. Despite varying flow rates, pC* remained constant, suggesting that the filtering ability of foam is dependent on the size of the particles, regardless of the influent turbidity.

Since horizontal filtration proved infeasible, it was decided to manipulate the required plan area geometry by instead increasing the down flow rate through the filter. Previous research showed it was also necessary to increase the filter depth in order to achieve effective performance.

Literature Review

Polyurethane foam filter/PAC adsorber

A foam filter consisting of small cubes of polyurethane foam is used to remove turbidity with three different foams at different degrees of compression, while monitoring the filter's clean bed head loss. Experiments demonstrated that the foam filter is capable of removing turbidity with results similar to that of sand and anthracite filters. Turbidity removal improved with an increase in foam compression and decrease in ppi. The run time increased with decreased compression and decreased ppi. The head loss for 15-ppi foam compressed 29% was 0.025 ft/ft, much less than the calculated sand head loss of 2 ft/ft. Powdered activated carbon (PAC) loaded in the filter acted as a fixed-bed adsorber and helped to reduce the levels of organic chemicals in water. These results are not directly applicable to our research, as we are using foam sheets, which utilize the porosity of the foam itself, rather than using foam cubes and compression to manipulate the porosity of the material. The loading of PAC into our filter to remove natural organic matter could be applicable to our design.

Coated Sand Filtration - An Emerging Technology for Water Treatment

Filtratio n media can be modifie d by using oxide coated sand in order to improv e their ability to remove heavy metals and other impuriti es from water. Studies found that "the iron and mangan ese oxides alone are not suitable as a filter mediu m because of their low hydraul ic conduct ivity." Hence, recent researc h has focused on

sorptive sand filtratio n using iron, alumin um, and mangan ese coasted sand. Ferric nitrate is best used as the source of iron if exposur e to mild abrasio n is possibl e due to backwashin g. Man у polluta nts and microor ganism s can be remove d from drinkin g water by utilizin g oxide coated sand. Lukasik experie nced a remova l of "greater than 99% of

E. coli, Vibrio cholera e poliovir us and colipha ge MS-2 from dechlor inated tap water." In additio n, alumin um and iron were both undetec ted in the effluent water after treatme nt, revealin g that the metallic hydroxi de coating is insolubl e. The metalloaded sand can be dispose d of as cemetiti ous solidifi cation, the "best demons trated availabl

e technol ogy for land disposa l of most toxic element s."

Open-Cell Polyurethane Foam (As a Filter Medium)

This article focused on using Polyurethane Foam as a filter medium for air. Though AguaClara is investigating using foam as a filter for water rather than air, the author, Collings, provides a strong background for us to build upon. Collings researched in great detail the process of manufacturing foam, calculating foam resistivity and permeability -information that our team can apply to our foam selection and calculations. Variables in Collings' experiment such as temperature, concentration, contact time and fluid velocity will probably effect our experiment as well. Similar to our current experiment, Collings mentions a big downfall in foam filtration is finding a method of cleaning the foam without execution downtime. Unfortunately he did not go into detail as to how this could be solved.

Potential of Silver Nanoparticle-Coated Polyurethane Foam as an Antibacterial Water Filter Silver and other such metal ions have shown signs of having antibact erial properti es without causing excessi ve harm to humans . For commu nities without access to major water purifica tion plants, silver nanoparticles can be an effective alternative (Jain 63). Another major upside to using silver nanoparticles is their resilience to washing cycles. According to the article, "There was no loss of nanoparticles after several washing and drying operations and after keeping it for several months in a closed environment" (Jain 62). Most importantly however, the silver nanoparticles greatly enhance the efficiency of the polyurethane foam by

successfully eliminating any residual pathogens (Jain 62). By using similar methods in soaking the AguaClara foam filters in aluminum hydroxide and sodium carbonate mix, the Foam Filtration Team hopes to meet similar success in eliminating all bacterial contaminants.

Detailed Task List

1. Perform a Performance Study of the 90 ppi polyurethane foam:

In order to characterize the performance of the foam, we will vary different variables while holding the others constant to find the optimal parameters to use for designing a foam filtration unit, and under what varied conditions the filter will still perform well. The variables we will study are Down flow Velocity(6, 12, 24 mm/s), Filter Depth (5, 10, 15 in), Turbidity(5, 10, 15 NTU), and Alum Dose(No or Yes).

	Velocity(mm/s)	Turbidity(NTU)	Depth(in)	Alum Dose	
	6	; 5	5	0	
	12	2 10	10	1	
	24	15	15		
	1.2	2			
Vary Flow:				Done?	Started
Experiment 1	6	i 5	10	1 YES	10-Jun
Experiment 2	12	2 5	10	1 YES	14-Jun
Experiment 3	24	5	10	1 Too High	l i i i i i i i i i i i i i i i i i i i
Vary Depth					
Experiment 4	6	i 5	15	1 YES	22-Jun
Experiment 5	6	5 5	10	1	
Experiment 6	6	; 5	5	1	
Experiment 7	12	2 5	15	1	
Vary Turbidity					
Experiment 8	6	i 10	10	1	
Experiment 9	6	i 15	10	1	
Vary Alum					
Experiment 10	6	; 5	10	0	
Headloss					

Experiment 11 Empty Column - No Filter

2. Calculate the head loss through the filter using a pressure sensor:

We have calculated the head loss through the filter using the Hagen-Poiseuille equation, which models the filter as a number of long thin pipes, but this does not seem correct. This may be due to an underestimation of the pore size used. Given the high porosity of the foam material, it is likely that the pore diameter should be larger than the value of 1/90 inch used in the calculation. Therefore, we will use pressure sensors to measure the headloss across the filter, as well as measure the head loss through an empty filter column(to calculate how much of the head loss is due to the flow through the fittings and tube) and subtract the two, resulting in the head loss across the filter. We will also measure head loss over time, to determine how long a filter can effectively be used for, before head loss is too great.

3. Determine the effectiveness of adding an Aluminum Hydroxide filter wash to the cleaning method: We may be able to achieve even greater filter performance by rinsing the filter in aluminum hydroxide prior to reinstallation in the filter column. Please see experimental methods section for preparation details. Additionally, it will be important to monitor the amount of residual alluminum in the effluent from the filter. This is an important parameter due to the potenially toxic effects of aluminum. The EPA secondary standard maximum contaminate level for aluminum is .05-.2 mg/L.

4. Determine the effect of Natural Organic Matter on the foam material, and its changed performance: Our experiments in the lab do not account for natural organic matter that will be in the water in AguaClara plants. Therefore, before we are able to implement any designs, we need to understand and account for the effects that the natural organic matter will have on the foam's filtering capacity, and associated method of cleaning.

5. Determine an efficient cleaning method for the filter:

It is necessary to detail a cleaning method for the foam material. This method should effectively remove particles and any bio matter, and simultaneously be easy for an operator to perform within a reasonable time frame.

6. Design a Foam Filtration Unit

This filtration unit design should be optimized according to the required surface area and filtration velocity parameters determined through previous laboratory experiments. In addition, it should minimize the required plan area, as well as maximize the ease of maintenance for the operator.

Experimental Design

Polyure thane foam has proven to be a potentia lly effectiv e means of filtratio n due to its small pore size, yet very high porosit y(. 969). The small pore size enables clay particle s to be capture d in the foam, while the high porosit y yields minima 1 head loss across the filter. These paramet ers allow a foam filter to achieve

a high particle remova l, even when run at very high flow rate. T his high flow rate results in a reduced require d plan area for a filtratio n unit.

In our experi ment we are currentl y using 90 pores per inch (ppi) foam in a 1 inch diamete r graduat ed cylinde r. One inch thick foam boards are cut using a band saw to fit the exact circumf erence of the cylinde r. Cutting the foam accurat ely is a crucial part of the experi ment. The foam must fit flush to the graduat ed cylinde

r to prevent prefere ntial flow around the foam through the cylinde r. A tight seal with all edges will force the water through the pores of the foam. Togeth er, the foam and graduat ed cylinde r act as our filter.

This summer , the first variable that the Foam Filtratio n team will test is foam thickne ss. We will test thickne sses 5, 10 and 15 inches. When placing the foam inside the graduat ed cylinde r, two things are crucial: consiste ncy in experi ment, and prevent ion of air bubbles . To maintai n consiste ncy, each 1 inch foam piece is number

ed in order of placem ent in the filter, and replace d in the same order each run. Great care is also taken in the placem ent of the individ ual filter layers. If the layers are pressed too close togethe r, the filter may become compre ssed, thus changin g the pore size of the filter, and making the data inconsi stent with other

experi mental trials. Dislodg ed air bubbles can create inconsi stency in data measur ement and interfer e with the filtratio n process.

The second variable we are analyzi ng is the effectiv eness of adding an Alumin um Hydrox ide /Sodiu m Carbon ate filter wash to the cleanin g method. The solution must be prepare d at the time of use to prevent the formati on of comple Х polyme rs in the solution . Our solution pH is maintai ned at roughly 7.0, the same pH as distilled

water. The solution needs to be saturate d with Alumin um Hydrox ide, but not so much that the precipit ate clogs our filter. The solution is prepare d by adding 5 mL of a 20 g/L Sodium Carbon ate solution to 50 mL of a 30 g /LAlumin um Hydrox ide solution . The first foam layer will not be soaked since it already capture s the majorit y of

particle s going through it—this layer does not need the extra filtering power. The last layer will not be soaked to reduce alumin um seepage into the effluent.

Before the experi ment begins, the Process Control ler must be set up to control our third and forth variable s: turbidit y and downw ard water velocity . The method controls the additio $n \ of$ clay solution to our influent 'raw water', as well as the pump that pulls water through our filter. The raw water simulat es the effluent from an

AguaCl ara plant. We will test our filter at influent concent rations of 5, 10 and 15 NTU, and down flow velociti es of 6, 12 and 24 mm /s.

After the foam layers have been placed in the cylinde r, the entire filter is secured into a clamp, joining it with the rest of the apparat us. The additio n of Alum is the fifth tested variable . Current ly, in active AguaCl ara plants, Alum is always added to the raw water supply. То determi ne the role that Alum plays in achievi ng effectiv

e perform ance in the foam filter, Alum will not be added to the raw water in some tests.

When connecting our experiment, we must ensure air is removed from both the filter column and all connected tubing. Air bubbles in the water supply can cause spikes in the pressure sensor and also result in inaccurate NTU readings. To remove these air bubbles, raw water must be sent into the filter from the opposite direction: in from the bottom of the filter and out through the top. Meanwhile, tubing of the raw water and the filtered water are connected to a pressure sensor to monitor head loss, the amount of energy required by the water to go through the foam.

When all air is remove d, the tubing is then connect ed in the proper directio n. Alu m will be added to the raw water prior to the filter by means of alum stock tank, where the amount added is determi ned by the filter down flow rate. T he alum is connect ed to the same pump as the effluent water, so an increas e in filter

flow rate results in a corresp onding increas e in alum. The raw water with alum is sent to the top of the filter, and flows through the foam before being pumped out through the bottom of the filter. This effluent filtered water is sent to a turbidi meter.

Both NTU and pressur e values are recorde d by Process Control ler every five seconds for both the raw and filtered water. Throug h these experi ments, the Foam Filtratio n team hopes to validate the filtering effectiv eness of foam, while achievi ng perform ance compar able to convent ional method s, yet requirin g less planned area.

Future Work

Over the next two weeks, our team will conduc t a variety of foam filtrati on experi ments while varyin g a specifi с parame ter for each trial. By changi ng one variabl e and holdin g others consta nt, our group can determ ine the optima 1 parame ters for designi ng a foam filtrati on

unit. Param eters that will be varied include down flow velocit у, filter depth, turbidit y, and alum dose. The foam current ly being used is set at 90 ppi (pores per inch) polyur ethane foam.

Please refer to the "Detail ed Task List" section for more inform ation on further experi ments schedu led to be comple ted by the end of this summe r.

All of these tasks and experi ments will be able to help us design the most favora ble and feasibl e foam filtrati on unit for AguaC lara plants. Based on our researc h, we will be able to better underst and the proces s of foam filtrati on and hopefu lly be able to imple ment the unit

easily into later plants.

Team Roles and Expectations

Team Expectations:

- Come to meetings when you can
- Remember Lab Safety
- Do your share of the work
- Complete work in a timely fashion (by the deadline..)

We will have a team meeting on Wednesdays at 5:00 pm in Hollister 150. In addition, we will meet up as a team to conduct experimental work as needed. Since the experiment run time varies for each experiment, it is difficult to say exact days and times when the experiment will be finished, and a new one can be set up to run. We will likely meet weekdays after 5, or in the afternoon depending on availability.

Team Roles: These roles will be rotated among team members with each experimental trial

- Experimental Setup This will entail cleaning out the filter from the previous experiment, replacing the filters in the filter column, and setting up the experiment to run again. Will also involve checking that the process control file is operating for the right flow rate and experiment time, and the data is being saved in the proper location.
- Experimental Maintenance/Operation This task will involve preparing an aluminum hydroxide sodium carbonate mixture to wash the filters in, refilling alum and clay stock tanks when necessary, and checking in on the experiment to ensure there are no leaks/failures in the system.
- Data Analysis After an experiment is complete, this task will entail compiling all of the data for the duration of the experiment from the datalog files into one text file, resolving any issues in it (replacing 0's and -999's) and loading the file into the Simple Data Analysis file in MathCAD.
- Wiki Editor After the data is analyzed for an experiment, it will be necessary to document the results and the implications on the Wiki so others will be able to easily find and understand the results.
- Team Leader (Sarah Stodter) Responsible for managing the team and experiments run, and ensuring assignments are completed on time, and the work load is evenly distributed amongst team members. Ensure that all team members understand the experimental set up, and reasoning, help troubleshoot problems, and provide guidance for the experiment.

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